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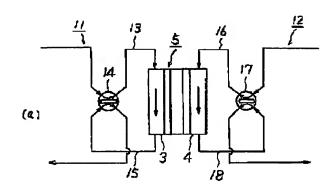
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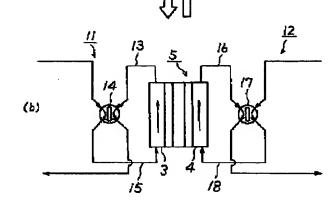
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TITLE

FUEL CELL POWER PLANT





ABSTRACT:

PURPOSE: To restrain deterioration of each cell as much as possible so as to prolong the life of a fuel cell main body by providing fuel-gas and oxidizer-gas lines which can switch the direction of fuel gas and that of oxidizer gas in each cell from normal to reverse.

CONSTITUTION: A fuel gas line 11 comprises a cell inlet pipe 13, a fuel gas switching valve 14 and a cell outlet pipe 15, and an oxidizer gas line 12 comprises a cell inlet pipe 16, an oxidizer gas switching valve 17 and a cell outlet pipe 18. When the body of the valve 14 passes through the pipe 13, the direction in which it moves is regarded as normal, whereas when the body passes through both of the pipes 13, 15 the direction in which it moves is regarded as reverse. During plant operation the valves 14 and 17 are controlled and switched from a normal to a reverse position or vice versa with the lapse of time. Therefore, the deteriorated portion of each cell is not specified and the life of a fuel cell main body can be prolonged.

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Notes

1. Untranslatable words are replaced with asterisks (****).

2. Texts in the figures are not translated and shown as it is.

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CLAIMS

[Claim(s)]

[Claim 1] In the fuel cell power generation plant which connects both gas stream ways so that it may have the fuel cell main part constituted by laminating many single batteries and oxidant gas may be sent for fuel gas to the fuel pole of said single battery on the oxidizer pole of said single battery. The fuel cell power generation plant characterized by preparing the fuel gas and the oxidant gas system which have the channel change means which can be switched to right reverse both directions for the fuel gas in said single battery, and the flow direction of oxidant gas.

DETAILED DESCRIPTION

[Detailed Description of the Invention]

[0001]

[Industrial Application] This invention relates to a fuel cell power generation plant. [0002]

[Description of the Prior Art] A fuel cell is a power generation means to obtain a direct electricity output from the electrochemical reaction produced on an electrode. In a fuel cell, in order to perform this electrochemical reaction continuously, you have to supply fuel gas and oxidant gas to the fuel pole and air pole which face each other on both sides of an electrolyte layer continuously, respectively.

[0003] An example of the composition of a fuel cell is shown in drawing 3. The fuel cell main part 1 is equipped with the single battery 5 which serves as the electrolyte layer 2 from the fuel pole 3 and the oxidizer pole 4 which are arranged by sticking to the both sides, and fuel gas 6 and oxidant gas 7 are supplied to both poles 3 and 4, respectively. Since many single batteries 5 are laminated and are constituted, the separator 8 for securing supply of each gas is used. This figure shows typically the fuel cell main part 1 with which fuel gas 6 and oxidant gas 7 are supplied to the single battery 5 as a parallel style or an opposite style. Both gas 6 and 7 flow and flow out in the direction perpendicular to Drawings. The mixed gas which generally uses hydrogen as main ingredients as oxidant gas 7 is used.

[0004] Oxygen and hydrogen react electrochemically within the single battery 5, and bring forth an electric output and steam. Since it reacts while hydrogen in fuel gas 6 and oxygen in oxidant gas 7 flow along with the single battery 5, both gas 6 and the molar fraction of hydrogen and oxygen in seven fall in the direction of a flow gradually. Moreover, since fuel gas 6 and oxidant gas 7 absorb generation of heat by the reaction, those temperature assumes the temperature gradient to which it goes up in the direction of a flow, and the single battery 5 also goes up in the direction of a flow of gas.

[0005] The Electrochemistry Sub-Division reaction becomes active, so that the

temperature of the single battery 5 is generally so high that the molar fraction of hydrogen in gas and oxygen is high. If the Electrochemistry Sub-Division reaction is active, the current density produced in the portion is large. Moreover, since the calorific value of the portion by reaction fever is large if the Electrochemistry Sub-Division reaction is active, the temperature of the portion becomes high easily. The single battery 5 shows distribution of temperature and current density by the synergy of both gas 6, and the concentration of 7 and the liveliness of a reaction.

[0006] The single battery 5 deteriorates easily in the field exposed to a field or high temperature with high current density. Therefore, degradation of the single battery 5 advances locally, while current density and temperature are [each other] related. [0007]

[Problem to be solved by the invention] Thus, since a fuel cell assumes the temperature distribution which is not uniform, and current density distribution, degradation may advance locally in the portion used as high temperature or high current density.

[0008] The fuel cell main part 1 is divided into a parallel style type, an opposite style type, and three rectangular style type form according to the flow direction of fuel gas 6 and oxidant gas 7. The single battery 5 has respectively characteristic temperature distribution and current density distribution according to such form.

[0009] Among these, it is thought that the single battery 5 has the feature which becomes high temperature easily locally as compared with the battery composition of other two form, and rectangular style type battery composition has an early advance of degradation. In order to make uniform temperature distribution of the single battery 5, and current density distribution, parallel style type battery composition is excellent, but a temperature gradient and a current density slope still cannot be made into zero. In order to aim at the reinforcement of a fuel cell, it is necessary to suppress local degradation of the single battery 5 to the minimum. Then, it is in the purpose of this invention offering the fuel cell power generation plant which controls degradation of a single battery as much as possible, and prolonged the life of the fuel cell main part.

[0010]

[Means for solving problem] This invention is equipped with the fuel cell main part constituted by laminating many single batteries in order to attain the above-mentioned purpose. In the fuel cell power generation plant which connects both gas stream ways so that oxidant gas may be sent for fuel gas to the fuel pole of a single battery on the oxidizer pole of a single battery It is characterized by preparing the fuel gas and the oxidant gas system which have the channel change means which can be switched to right reverse both directions for the fuel gas in a single battery, and the flow direction of oxidant gas.

[0011]

[Function] The principle of this invention is explained with reference to drawing 2. [0012] This is what was applied to the parallel style type fuel cell main part 1, and other opposite style types and a rectangular cross style type are also the same. With the separator 8, it is divided mutually and fuel gas 6 and oxidant gas 7 are flowing through both sides of the single battery 5 in parallel. In (a), any gas is flowing into this side from back, and temperature is high in this side and it is in the tendency for the single battery 5 to have high temperature distribution by the lower stream side of gas similarly. Since the reaction ingredient of gas is reduced in the direction of a flow, the density of the current produced by a reaction changes in the direction of a flow. Furthermore, current density changes depending on the capacity factor and gas temperature of gas. Therefore, the degradation speed of the single battery 5 changes by the upper stream [of gas], and lower stream side with the temperature distribution of the single battery 5, and current

density distribution, and the life of the single battery 5 is restricted in the early portion of degradation.

[0013] Then, by a channel change means, as shown in (b), the flow direction of both gas is switched to back from this side. It means that the temperature distribution and density distribution of the single battery 5 settle in different distribution from change before, and the portion with temperature and the current density conditions of being easy to deteriorate in the single battery 5 had moved them, being dependent also on distribution about degradation. After a certain time progress, again, if the flow direction of gas is reversed, depending on distribution about degradation of the single battery 5, temperature distribution and current density distribution will change and will move the part which deteriorates easily.

[0014] Thus, by switching the flow direction of gas to the both directions which have the relation of a right contrary, the degradation portion of the single battery 5 is not specified as a certain position, but it is lost that the life of the single battery 5 will be restricted by only degradation of the position. Therefore, the life of the fuel cell main part 1 can be prolonged.

[0015]

[Working example] One example of this invention is hereafter explained with reference to drawing 1 (a) and (b). The fuel gas system 11 is connected to the fuel pole 3 of the single battery 5, and the oxidant gas system 12 is connected to the oxidizer pole 4 of the single battery 5.

[0016] The fuel gas system 11 consists of a battery entrance pipe 13, and the fuel gas change-over valve 14 and the battery outlet pipe 15, and the oxidant gas system 12 consists of a battery entrance pipe 16, and the oxidant gas change-over valve 17 and the battery outlet pipe 18 similarly.

[0017] The fuel gas change—over valve 14 can be arranged in the position where the battery entrance pipe 13 and the battery outlet pipe 15 cross as shown in a figure, and a mutual course can be opened for free passage now. It can arrange to the oxidant gas change—over valve 17 in the position where the battery entrance pipe 16 and the battery outlet pipe 18 cross similarly, and a mutual course can be opened for free passage. [0018] In the above—mentioned composition, the valve element of the fuel gas change—over valve 14 in (a) is opening battery entrance pipe 13 comrades for free passage, and makes this a positive style position. Moreover, in (b), the battery entrance pipe 13 and the battery outlet pipe 15 are opened for free passage, and let this be an adverse current position. Similarly, the valve element of the oxidant gas change—over valve 17 of (a) is opening battery entrance pipe 16 comrades for free passage, and makes this a positive style position. In (b), the battery entrance pipe 16 and the battery outlet pipe 17 are opened for free passage, and let this be an adverse current position.

[0019] During operation of a fuel cell power generation plant, the fuel gas change-over valve 14 and the oxidant gas change-over valve 17 are operated, and from a positive style position, it switches to a positive style position with progress of time from an adverse current position again, and goes to an adverse current position.

[0020] The portion which has by this temperature and the current density conditions of being easy to deteriorate in the single battery 5 with time can be moved, and it becomes possible to lose that the life of the single battery 5 receives restriction only by degradation.

[0021]

[Effect of the Invention] As explained above, since this invention switched the fuel gas in a single battery, and the flow direction of oxidant gas to right reverse both directions, it is lost that the degradation part of a single battery is specified of it, and it does so the

outstanding effect that the life of a fuel cell main part is e	xtensible.
[Translation done.]	

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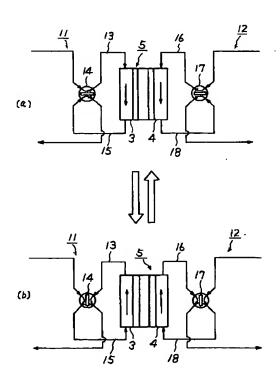
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(54)【発明の名称】 燃料電池発電プラント

(57)【要約】

【目的】 単電池の劣化を可能な限り抑制し、燃料電池 本体の寿命を延ばすこと。

【構成】 燃料ガス系統11には電池入口管13と、燃料ガ ス切換弁14と電池出口管15とが備えられ、また、酸化剤 ガス系統12には電池入口管16と、酸化剤ガス切換弁17と 電池出口管18とが備えられる。燃料ガス切換弁14は電池 入口管13と電池出口管15とが交差する位置にある。ま た、酸化剤ガス切換弁17は電池入口管16と電池出口管18 とが交差する位置にある。



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【特許請求の範囲】

【請求項1】 単電池を多数積層して構成される燃料電池本体を備え、燃料ガスを前記単電池の燃料極に、酸化剤ガスを前記単電池の酸化剤極へ送るように双方のガス流路を接続してなる燃料電池発電プラントにおいて、前記単電池内の燃料ガスおよび酸化剤ガスの流動方向を正逆両方向に切換可能な流路切換手段を有する燃料ガスおよび酸化剤ガス系統を設けたことを特徴とする燃料電池発電プラント。

【発明の詳細な説明】

[0001]

【産業上の利用分野】この発明は燃料電池発電プラント に関する。

[0002]

【従来の技術】燃料電池は電極上で生じる電気化学的反応から、直接電気出力を得る発電手段である。燃料電池において、この電気化学的反応を継続的に行うには、燃料ガスと酸化剤ガスとを電解質層を挟んで向かい合う燃料極と空気極とに、それぞれ継続的に供給しなければならない。

【0003】燃料電池の構成の一例を図3に示す。燃料電池本体1は電解質層2と、その両面に密着して配置される燃料極3および酸化剤極4とからなる単電池5を備え、双方の極3、4にそれぞれ燃料ガス6と酸化剤ガス7とが供給される。単電池5は多数積層して構成されるので、それぞれのガスの供給を確保するためのセパレータ8が使用される。本図は燃料ガス6と酸化剤ガス7とが並行流あるいは対向流として単電池5に供給される燃料電池本体1を模式的に示したものである。双方のガス6、7は図面に垂直な方向に流入、流出する。燃料ガス6としては一般に水素を主要な成分とする混合ガスが用いられ、酸化剤ガス7としては一般に酸素を主要な成分とする混合ガスが用いられる。

【0004】酸素と水素は単電池5内で電気化学的に反応し、電気出力と水蒸気とを産み出す。燃料ガス6中の水素および酸化剤ガス7中の酸素が単電池5に沿って流れながら反応するので、双方のガス6、7中の水素と酸素のモル分率は流れ方向に徐々に低下する。また、燃料ガス6および酸化剤ガス7がその反応による発熱を吸収するので、それらの温度は流れ方向に上昇し、単電池5もガスの流れ方向に上昇する温度勾配を呈する。

【0005】一般に、ガス中の水素および酸素のモル分率が高いほど、また単電池5の温度が高いほど、電気化学反応は活発になる。電気化学反応が活発であれば、その部分で生じる電流密度は大きい。また、電気化学反応が活発であれば、反応熱によるその部分の発熱量は大きいので、その部分の温度は高くなり易い。双方のガス6、7の濃度と反応の活発さの相乗作用によって単電池5は温度および電流密度の分布を示す。

【0006】単電池5は電流密度の高い領域あるいは高

温にさらされる領域において劣化し易い。したがって、 単電池5の劣化は電流密度と温度が互いに関係し合うな かで局所的に進行する。

[0007]

【発明が解決しようとする課題】このように燃料電池は 運転中、燃料電池本体1に組み込まれた単電池5が一様 でない温度分布と電流密度分布を呈するため、高温ある いは高電流密度となる部分で局所的に劣化が進行するこ とがある。

【0008】燃料ガス6と酸化剤ガス7との流動方向に従い、燃料電池本体1は、並行流型、対向流型、直交流型の3型式に分けられる。これらの形式によって単電池5はそれぞれ特有な温度分布と電流密度分布を有する。

【0009】このうち直交流型の電池構成は他の2型式の電池構成に比較して単電池5が局所的に高温になり易い特徴をもち、劣化の進行が早いと考えられている。単電池5の温度分布および電流密度分布を一様にするためには並行流型の電池構成が優れているが、それでも温度勾配および電流密度勾配を零にすることはできない。燃料電池の長寿命化を目指すには、単電池5の局所的な劣化を最小限に抑える必要がある。そこで、本発明の目的は単電池の劣化を可能な限り抑制し、燃料電池本体の寿命を延ばすようにした燃料電池発電プラントを提供することにある。

[0010]

【課題を解決するための手段】上記目的を達成するために本発明は、単電池を多数積層して構成される燃料電池本体を備え、燃料ガスを単電池の燃料極に、酸化剤ガスを単電池の酸化剤極へ送るように双方のガス流路を接続してなる燃料電池発電プラントにおいて、単電池内の燃料ガスおよび酸化剤ガスの流動方向を正逆両方向に切換可能な流路切換手段を有する燃料ガスおよび酸化剤ガス系統を設けたことを特徴とする。

[0011]

【作用】本発明の原理を図2を参照して説明する。

【0012】これは並行流型の燃料電池本体1に応用したもので、他の対向流型、直交流型も同様である。燃料ガス6および酸化剤ガス7は単電池5の両面をセパレータ8によって互いに仕切られて並行に流れている。

(a)においては、いずれのガスも後方から手前に流れており手前で温度が高く、単電池5も同様にガスの下流側で高い温度分布をもつ傾向にある。ガスの反応成分は流れ方向に低減するので、反応により生じる電流の密度は流れ方向に変化する。さらに、電流密度はガスの利用率とガス温度に依存して変化する。したがって、単電池5の劣化速度は単電池5の温度分布と電流密度分布によってガスの上流側と下流側とで異なり、単電池5の寿命は劣化の早い部分で制限される。

【0013】そこで、流路切換手段によって(b)に示すように双方のガスの流動方向を手前から後方へと切換

える。単電池5の温度分布と密度分布とは劣化程度の分布にも依存しながら、切換え前とは異なった分布に落ち着き、単電池5の中で劣化しやすい温度および電流密度条件をもつ部分は移動したことになる。ある時間経過後、再度、ガスの流動方向を逆転すると、単電池5の劣化程度の分布に依存して、温度分布と電流密度分布とは変化し、劣化し易い箇所は移動する。

【0014】このように、ガスの流動方向を正逆の関係にある両方向に切換えることにより、単電池5の劣化部分はある位置に特定されず、その位置の劣化のみによっ 10 て単電池5の寿命が制限されてしまうことがなくなる。したがって、燃料電池本体1の寿命を延ばすことができる。

[0015]

【実施例】以下、本発明の一実施例を図1(a)(b)を参照して説明する。燃料ガス系統11は単電池5の燃料極3に、また酸化剤ガス系統12は単電池5の酸化剤極4に接続されている。

【0016】燃料ガス系統11は電池入口管13と、燃料ガス切換弁14と電池出口管15とから構成され、同様に酸化 20 剤ガス系統12は電池入口管16と、酸化剤ガス切換弁17と電池出口管18とからなる。

【0017】図に示す如く電池入口管13と電池出口管15とが交差する位置に燃料ガス切換弁14を配置して互いの経路を連通することができるようになっている。同様に電池入口管16と電池出口管18とが交差する位置に酸化剤ガス切換弁17に配置して互いの経路を連通することができる。

【0018】上記構成において、(a)における燃料ガス切換弁14の弁体は電池入口管13同士を連通しており、これを正流位置とする。また(b)においては電池入口

管13と電池出口管15とを連通しており、これを逆流位置とする。同様に、(a)の酸化剤ガス切換弁17の弁体は電池入口管16同士を連通しており、これを正流位置とする。(b)においては電池入口管16と電池出口管17とを連通しており、これを逆流位置とする。

【0019】燃料電池発電プラントの運転中、燃料ガス 切換弁14および酸化剤ガス切換弁17を操作して正流位置 から逆流位置へ、また、逆流位置から正流位置へと時間 の経過と共に切換えて行く。

【0020】これにより、時間と共に単電池5の中で劣化しやすい温度および電流密度条件をもつ部分を移動させることができ、劣化のみによって単電池5の寿命が制限を受けるのをなくすことが可能になる。

[0021]

【発明の効果】以上説明したように本発明は、単電池内の燃料ガスおよび酸化剤ガスの流動方向を正逆両方向に切換えるようにしたので、単電池の劣化部が特定されることがなくなり、燃料電池本体の寿命を延長できるという優れた効果を奏する。

【図面の簡単な説明】

【図1】本発明による燃料電池発電プラントの一実施例 を示す構成図。

【図2】本発明の動作原理を説明するための図。

【図3】従来の燃料電池本体の一例を示す断面図。

【符号の説明】

5…単電池

11…燃料ガス系統

12…酸化剤ガス系統

14…燃料ガス切換弁

17…酸化剤ガス切換弁

[図3]

